

**REMARKS**

This is a full and timely response to the outstanding non-final Office Action mailed November 2, 2005 (Paper No. 103005). Upon entry of this response, claims 46-50 are pending in the application. In this response, claim 46 and 50 have been amended. Applicants respectfully requests that the amendments being filed herewith be entered and request that there be reconsideration of all pending claims.

1. Rejection of Claims 48 and 49 under 35 U.S.C. §112, Second Paragraph

Claims 48 and 49 have been rejected under 35 U.S.C. §112, second paragraph, as being indefinite for failing to particularly point out and distinctly claim the subject matter which Applicants regard as their invention. The Office Action states that:

Specifically, the language within lines 4 and 5 of claim 48 is unclear with respect to what is being reacted. The language “reacting a compound obtained by reacting a compound (eb) with a compound (fb) and further reacting with a compound (i)”, is confusing, because it cannot be determined what is being initially reacted with the “obtained” compound, since compound (i) is claimed as being “further” reacted. In other words, there appears to be too many occurrences of “reacting.”  
(Office Action, p. 2)

Independent claim 48 is amended to further clarify the subject matter which Applicants regard as their invention. Applicants respectfully submit that the amendment overcomes the rejection of claims 48 and 49, and requests that the rejection be withdrawn.

2. Rejection of Claims 46 and 47 under 35 U.S.C. §103

Claims 46 and 47 have been rejected under §103(a) as allegedly obvious over *Barron* (U.S.4,067,844) or *Zwiener* (U.S. 5,364,955). Applicant respectfully traverses the rejection of claims 46 and 47. It is well established at law that, for a proper rejection of a claim under 35 U.S.C. §103 as being obvious based upon a combination of references, the cited combination of

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references must disclose, teach, or suggest, either implicitly, all elements/features/steps of the claim at issue. *See, e.g., In re Dow Chemical*, 5 U.S.P.Q.2d 1529, 1531 (Fed. Cir. 1988); *In re Keller*, 208 U.S.P.Q.2d 871, 881 (C.C.P.A. 1981).

a. Claim 46

The Office Action takes the position that “the respective processes [of *Barron* and *Zwiener*] yield the same product and the only difference amounts to changing the sequence of steps in a multi-step process, and it has been held that such a modification is obvious where an unexpected result is not obtained.” (Office Action, p. 3, section 4.) As will be explained in more detail below, Applicants respectfully disagree with this characterization of the references as yielding the same product as claims 46 and 47.

1) *Barron* and *Zwiener* Produce a Side Reaction

As argued in the last Office Action, both *Barron* and *Zwiener* disclose that a prepolymer is produced in step (2) of their respective processes. Applicants also argued that because a prepolymer is produced a side reaction such as dimerization and trimerization of urethane prepolymer inevitably occurs, so that a product produced by *Barron* or *Zwiener* has high molecule and high viscosity. (See Response filed Aug. 3, 2005, p. 8). In contrast, the process of claim 46 dispenses with the step of producing a prepolymer, and a product of claim 46 has low viscosity. Thus, the process of claim 46 differs in a non-obvious way from the processes disclosed in *Barron* and *Zwiener*.

The outstanding Office Action stated that Applicants’ arguments about side reactions were unsubstantiated opinion, since no evidence or logical rationale was provided to support Applicants’ position. (Office Action, p. 4.) Applicants provide herein both logical rationale and experimental data supporting Applicants’ position with regard to side reactions.

In a reaction process like *Barron* and *Zweiner*, when a polyisocyanate is reacted with a polyol, a prepolymer is produced. If this reaction progresses ideally, the NCO terminated prepolymer (basic unit) is obtained with reaction of two polyisocyanate molecules and one polyol molecule. However, as shown by experimental data in Appendix A-1, a dimer (double unit) and trimer (triple unit) which has twice or three times of molecular weight are also produced by side reactions, due to both polyisocyanate and polyol being multi-functional compounds. Accordingly, the final prepolymer product contains a large amount of high weight molecule.

This is evidenced by the experimental data presented in Appendices A and B. Appendix A is a Japanese language article from a 1996 issue of “Adhesion Technology Japan”, and Appendix B is the English translation of Table 3-18. Dimerization and trimerization in prepolymer production are clearly seen in the data of Appendix A/B, which will now be explained in detail. Table 3.18 shows the GPC (Gel Permeation Chromatography) charts of the prepolymer, with various isocyanate group contents which have been obtained using the same polyol (molecular weight 3000 of PPG) and polyisocyanate (polymeric MDI). In the Table, “iso monomer” means isocyanate monomer, “iso dimer” means dimer of isocyanate, “iso trimer” means trimer of isocyanate, “iso tetramer” means tetramer of isocyanate, “basic unit” means monomer or basic unit (prepolymer), “pre dimer” means dimer (double unit) of prepolymer, and “pre trimer” means trimer (triple unit) of prepolymer.

In the Table, chart (a) shows the prepolymer (15% isocyanate group content) which is obtained by 2:1 reaction with NCO group of polyisocyanate and OH group of polyol. Even in such prepolymer prepared at the theoretical reacting ratio, peak (7) of “pre dimer (double unit)” is observed. Further, as the isocyanate group content in the prepolymer is decreased from 15% to

6% the content of “pre dimer (double unit)” (7) and “pre trimer (triple unit)” (8) is increased. In any case where isocyanate group content is 15%, 9% or 6%, the dimer and/or trimer exist in the prepolymer product.

In other words, the side reaction, that is, production of dimerization and trimerization, *inevitably* occurs in producing a prepolymer by reacting a polyisocyanate with a polyol. Accordingly, an actual pre-polymer composition has higher molecule weight and higher viscosity than those of the ideal basic unit. Also, the final product or resin compositions, which use the prepared prepolymer as raw materials, have high viscosity. As is apparent from the above, the occurrence of side reactions is already known, and is supported by Appendix A/B.

The process of claim 46 therefore differs in a non-obvious way from the processes disclosed in *Barron* and *Zwiener*. Accordingly, a *prima facie* case establishing an obviousness rejection under *Ex parte Rubin* has not been made. For at least these reasons, claim 46 is not obvious over *Barron* or *Zwiener*, and the rejection should be withdrawn.

2) *Barron* and *Zwiener* Produce a Different Product than Claim 46

As argued in the last Office Action, according to the process disclosed in *Barron* and *Zwiener*, the urethane polymer has a hydrolysable silyl group and a NCO group in the terminal. On the other hand, the product of claim 46 has a hydrolysable silyl group and an OH group in the terminal. (See Response filed Aug. 3, 2005, pp. 8-9.) Thus, the products of *Barron* and *Zwiener* are different from the product of claim 46.

The outstanding Office Action stated that “applicants’ arguments are largely based upon the position that the instant products have an OH group in the terminal; however, applicants’ claims are not so limited. There is no requirement that such a terminal OH group exists or be produced.” (Office Action, p. 4.) Applicants provide herein a logical rationale supporting Applicants’ position.

Considering the process of the reaction, it is clear to one of ordinary skill in the art that the product by the process of claim 46 necessarily contains hydrolysable silyl group terminated polymer, and may in some circumstances contain OH group terminated polymer. However, applicants do not limit the product of claim 46 to the products having a terminal OH group. Applicants' reference to the "OH group" in the last response was made to emphasize the difference from *Barron* and *Zwiener*. The final product of claim 46 is hydrolysable silyl group terminated polymer, and if all ends of polyol do not react, the product may have a terminal OH group. That is simply an issue of possibility or probability.

Specifically, the process of Claim 46 comprises (1) obtaining a silicon compound (product (N)) having an active hydrogen being reactive with a isocyanate group, (2) reacting the product (N) with a compound (G) having an NCO group to obtain a silicon compound (product (O)) having a NCO group, and (3) reacting the product (O) with a compound having an OH group. The final product is hydrolysable silyl group terminated polymer. and if all ends of polyol do not react, the product may have a terminal OH group. See Appendix C.

In contrast, reactions in the references are different from the present invention. The process of *Barron* comprises the steps of (1) obtaining an aminosilane, (2) reacting a polyol compound with a polyisocyanate compound to produce a urethane prepolymer, and (3) reacting the aminosilane with the urethane prepolymer. (Col. 2, lines 59-66 and Col. lines 37-50.) The final product contains components of higher molecule weights and has hydrolysable silyl group, but it cannot possibly have a terminal OH group. See Appendix E.

Further, the process of *Zwiener* comprises the steps of (1) reacting a polyol compound with a polyisocyanate compound to produce a urethane prepolymer, (2) obtaining an aminosilane, and (3) reacting the amino silane with the urethane prepolymer (Examples 5 and 8).

The final product contains components of higher molecule weights and has hydrolysable silyl group, but cannot possibly have a terminal OH group. See Appendix F.

In summary, none of the cited references disclose, teach, or suggest the product of claim 46.

b. Claim 47

Since independent claim 46 is allowable, Applicants respectfully submit that claim 47 is allowable for at least the reason that it depends from an allowable claim. *In re Fine*, 837 F.2d 1071, 5 U.S.P.Q. 2d 1596, 1598 (Fed. Cir. 1988). Therefore, Applicants respectfully request that the rejection of claim 47 be withdrawn.

3. Rejection of Claim 50 under 35 U.S.C. §103

Claim 50 has been rejected under §103(a) as allegedly obvious over *Krafcik* (U.S. 5,614,604). Applicants respectfully submit that the claim amendments made herein overcome the objection. It is well established at law that, for a proper rejection of a claim under 35 U.S.C. §103 as being obvious based upon a combination of references, the cited combination of references must disclose, teach, or suggest, either implicitly, all elements/features/steps of the claim at issue. *See, e.g., In re Dow Chemical*, 5 U.S.P.Q.2d 1529, 1531 (Fed. Cir. 1988); *In re Keller*, 208 U.S.P.Q.2d 871, 881 (C.C.P.A. 1981).

1) *Krafcik* Produces a Side Reaction

In a reaction process like *Krafcik*, when a polyisocyanate is reacted with a polyol, a prepolymer is produced. If this reaction progresses ideally, the NCO terminated prepolymer (basic unit) is obtained with reaction of two polyisocyanate molecules and one polyol molecule. However, as shown by experimental data in Appendix A-1, a dimer (double unit) and trimer (triple unit) which has twice or three times of molecular weight are also produced by side

reactions, due to both polyisocyanate and polyol being multi-functional compounds.

Accordingly, the final prepolymer product contains a large amount of high weight molecule.

This is evidenced by the experimental data presented in Appendices A and B, introduced above. In Table 3-18 of Appendix A/B, chart (a) shows the prepolymer (15% isocyanate group content) which is obtained by 2:1 reaction with NCO group of polyisocyanate and OH group of polyol. Even in such prepolymer prepared at the theoretical reacting ratio, peak (7) of “pre dimer (double unit)” is observed. Further, as the isocyanate group content in the prepolymer is decreased from 15% to 6% the content of “pre dimer (double unit)” (7) and “pre trimer (triple unit)” (8) is increased. In any case where isocyanate group content is 15%, 9% or 6%, the dimer and/or trimer exist in the prepolymer product.

In other words, the side reaction, that is, production of dimerization and trimerization, *inevitably* occurs in producing a prepolymer by reacting a polyisocyanate with a polyol. Accordingly, an actual pre-polymer composition has higher molecule weight and higher viscosity than those of the ideal basic unit. Also, the final product or resin compositions, which use the prepared prepolymer as raw materials, have high viscosity. As is apparent from the above, the occurrence of side reactions is already known, and is supported by Appendix A/B.

Because a prepolymer is produced a side reaction such as dimerization and trimerization of urethane prepolymer inevitably occurs, so that a product produced by *Krafcik* has high molecule weight and high viscosity. In contrast, the process of claim 50 dispenses with the step of producing a prepolymer, and a product of claim 50 has low viscosity. Thus, the process of claim 50 differs in a non-obvious way from the processes disclosed in *Krafcik*. Accordingly, a *prima facie* case establishing an obviousness rejection under *Ex parte Rubin* has not been made.

For at least these reasons, claim 50 is not obvious over *Krafcik*, and the rejection should be withdrawn.

2) *Krafcik* Produces a Product without a Terminal OH Group

As argued in the last Office Action, according to the process disclosed in *Krafcik*, the terminal of the polymer of *Krafcik* is hydrolysable silyl group, or an alkyl group connected with a urethane linkage, and the hydrolyzed silyl group is hydrolyzed with water. In contrast, the terminal of the product of claim 50 is a hydrolysable silyl group and an OH group. (See Response filed Aug. 3, 2005, pp. 8-9). Thus, the product of *Krafcik* is different from the product of claim 50.

The outstanding Office Action stated that “applicants’ arguments are largely based upon the position that the instant products have an OH group in the terminal; however, applicants’ claims are not so limited. There is no requirement that such a terminal OH group exists or be produced.” (Office Action, p. 4.) Applicants provide herein a logical rationale supporting Applicants’ position.

Considering the process of the reaction, it is clear to one of ordinary skill in the art that the product by the process of claim 50 necessarily contains hydrolysable silyl group terminated polymer, and may in some circumstances contain OH group terminated polymer. However, Applicants do not limit the product of claim 50 to the products having a terminal OH group. Applicants’ reference to the “OH group” in the last response was made to emphasize the difference from *Krafcik*. The final product of claim 50 is hydrolysable silyl group terminated polymer, and if all ends of polyol do not react, the product may have a terminal OH group. This is simply an issue of possibility or probability.

In contrast, reactions in the references are different from the present invention. The process of *Krafcik* comprises the steps of (1) producing a urethane prepolymer, (2) reacting an



NCO group of the urethane prepolymer with an alcohol and an aminosilane, and (3) charging water (Col. 5, line 31 to Col. 6, line 9). The final product has no terminal OH group. The final product contains components of higher molecule weights and has hydrolysable silyl group, but it cannot possibly have a terminal OH group. See Appendix G. In summary, *Krafcik* does not disclose, teach, or suggest the product of claim 50.

3) Amended Claim 50 Produces a Moisture Curable Product

Applicants argued in the last response that the product of claim 50 differs from the product of *Krafcik* in that *Krafcik* is directed to a polyurethane dispersion, while the product of claim 50 is directed to a moisture curable product. The outstanding Office Action indicated that Applicants' argument "does not distinguish the claim from the prior art. Nothing in applicants' claim requires the product to be moisture curable...The claim is open to virtually any step or modification." (Office Action, p. 5, section 8.)

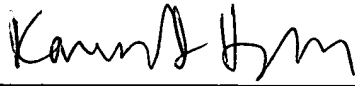
Claim 50 has been amended to recite "A process for the preparation of *moisture curable* urethane resins..." Therefore, even if Applicants' claimed process was analogous to changing a sequence of steps, Applicants' claimed process produces unexpected results. Therefore, a *prima facie* case establishing an obviousness rejection under *Ex parte Rubin* has not been made. For at least these reasons, claim 50 is not obvious over *Krafcik*, and the rejection should be withdrawn.

**CONCLUSION**

Applicants respectfully request that all outstanding objections and rejections be withdrawn and that this application and presently pending claims 46-50 be allowed to issue. If the Examiner has any questions or comments regarding Applicants' response, the Examiner is encouraged to telephone Applicants' undersigned counsel.

Respectfully submitted,

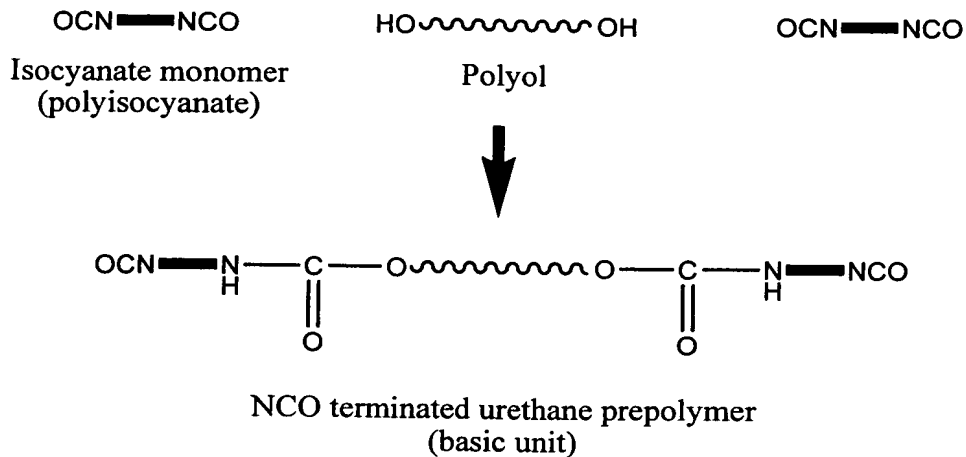
**THOMAS, KAYDEN, HORSTEMEYER  
& RISLEY, L.L.P.**

By:   
**Karen G. Hazzah, Reg. No. 48,472**

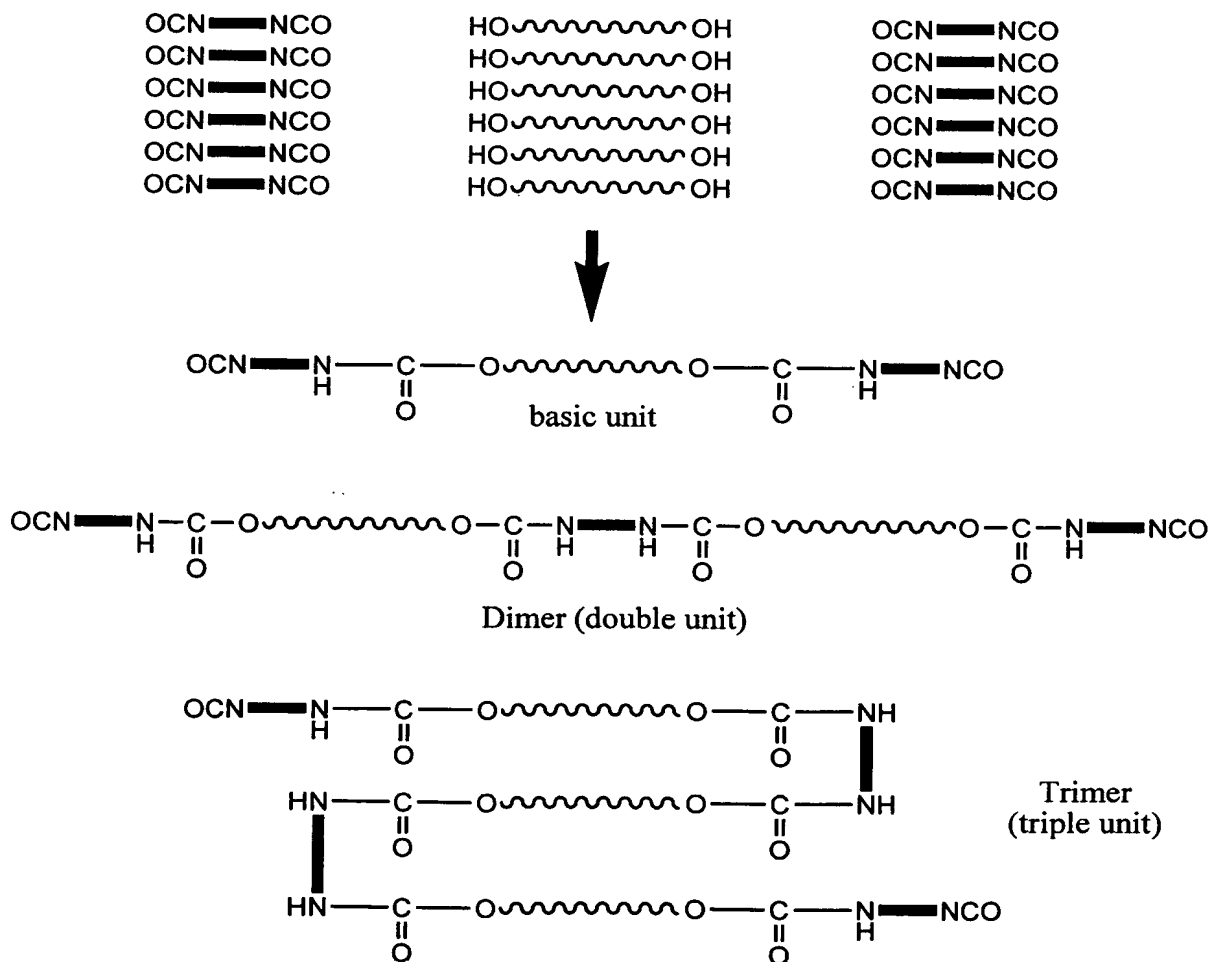
100 Galleria Parkway, NW  
Suite 1750  
Atlanta, Georgia 30339-5948  
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Fax: (770) 951-0933

## Appendix A-1

Ideal Reaction [NCO : OH = 2 : 1]



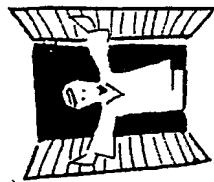
Side Reaction (Actual Reaction) [NCO : OH = 2 : 1]



大阪では、天神祭前後が最も暑いというのが定説。今年もまた冷夏かと思われた夏  
の入りも、土用を過ぎた頃から連日の猛暑、天神祭も本来の暑さのなかでの「コンチ  
キチ」と、やっと夏らしさのなかで高校野球のシーズン到来。

本号は、粘着および粘着加工品について特集しました。粘着剤および粘着加工品のメーカーのペタランの方に意見を頼みました。ちょっと話題の現況性はきいていても取り上げてみました。粘着テープの試験法についての解説も含まれています。これ一冊でユーザーの方々に粘着製品の隅隅を理解していただけたらと思います。

この特集号が発行されるころには、秋風が吹いているかも知れませんが、でも秋気はホットに上昇してはいいものです。(1995. 7. 30) (三刀基郷)



讀者の皆様へ

「接客の技術」をより身近なものにして頂くために、ご寄  
樹やご意見を是非お寄せ下さい。

次号は1月に特集「土木工事と接巻」を予定

致しております。ご期待下さい。

## 接 着 の 技 術 監 査

[illegible]

# 技の着衣

## 特集：ウレタン系接着剤

Vol. 15 No. 3 1996

発行：

日本接着學會





モノマー・ジイソシアネートは芳香族と脂肪族系があり芳香族系はポリオールとの反応が速く反応力も大きいが硬化物は質変しやすい。脂肪族系はポリオールとの反応は速く硬化物の弾力性も小さいが質変は無い。

ポリオールは官能基数と分子量が使用に当たってのポイントであり官能基数が低いと接着剤硬化物の弾力性は上がるが引裂に弱くなる。逆に低いと硬化物の伸度は大きくなるが弾力性は低下する。分子量の大きなポリオールを使用するとガラス転移点の低い柔軟な硬化物が得られるが弾力性は低下する。

プレポリマーの構造と硬さの関係を図3.16に、原料ポリオールとウレタンプレポリマーの性状についてを表3.17に、ゲル化・ミエーシン・クロマトグラフ (GPC) からみたダイアジン・グレートポリマーとはどのようなものかを表3.18に示す。

空気中あるいは溶液中の水分と反応して硬化する一液型気硬化型ウレタン系接着剤の硬化機構を図3.20に示す。

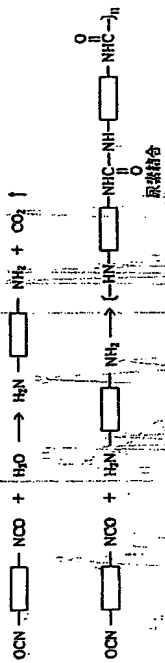


図3.20 ウレタンプレポリマーと水の反応

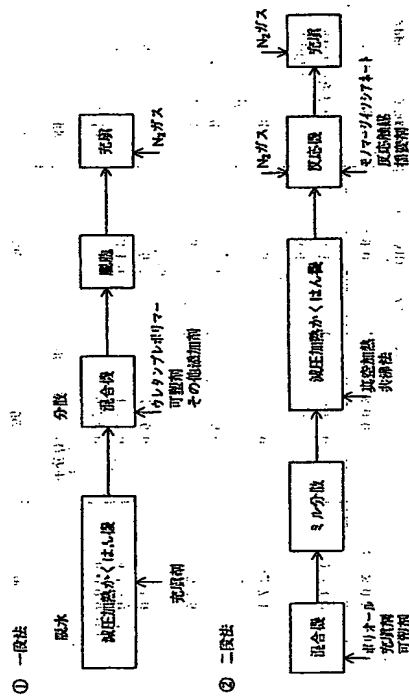


図3.21 一液型気硬化型ウレタン系接着剤製造工程

### 3.3.3 一液型気硬化型ウレタン系接着剤の製造方法

一液型気硬化型ウレタン系接着剤の製造に際して最も重要なことは水分の除去である。単に使用する充填剤に吸着している水分は接着剤の貯蔵安定性を低下させるので製造工程で除去しなければならない。製造方法としては加熱減圧脱水処理しない。原料ポリオールとウレタンプレポリマーを2割ミキサー、プラネター、ミキサー等で混練し仕上げる2段階と予めポリオールと充填剤等を混合加熱減圧脱水後モノマー・ジイソシアネートを加えて反応プレポリマー化してゆき1段階とがある。一般的な製造工程を図3.21に示す。

### 3.3.4 一液型気硬化型ウレタン系接着剤の問題点

一液型気硬化のため充填剤の乾燥はいうまでもなく水分と反応して炭酸ガスの発生を伴う用途により外観を損なう事や接着力の安定性に悪影響を及ぼす。

す。このために発泡抑制剤が必要となる。通常その対策としては脱水剤 (モレキュラーシーブ・ケイ素土・合成ケイ酸塩・無水石膏等) 炭酸ガス吸収剤として微粒子生石灰等が使用される。その他ベースプレポリマーのポリオールの組成・イソシアネート基含有率の影響もみのがせない。又熱硬化システムによる対策も検討されている。図3.22は応用可能な一

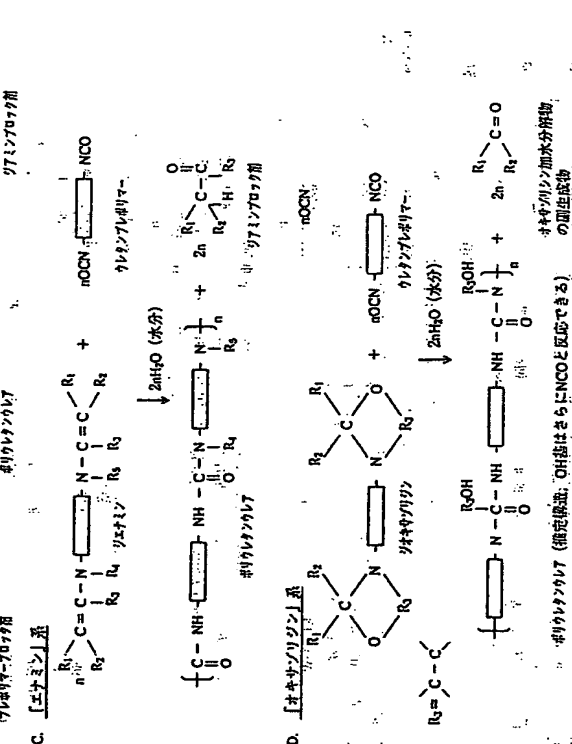
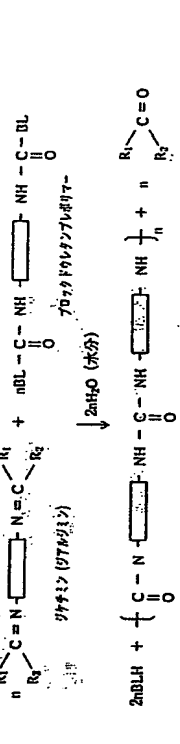
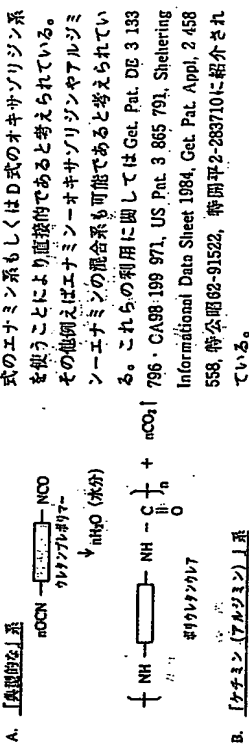


図3.22 接着剤接着剤、シーラントに適用可能な気硬化型ウレタン系接着剤の製造工程

[illegible]

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第319一 物理与化学利用ラタン器接装の性能

項目	KU9055/W	パナ用 KU-1	KU810P/PS
外観	乳白色ペー スト	黄白色ペー スト	所蔵色ペー スト
色相	95B1	100	95B1
粘度	11000 (S)	100000	17000 (S)
比重	1.1100 (20℃)	1.5-1.6	12000 (W)
使用法	1.55±0.1 キシリチン/ナ シ	ナシ/ナシ	1.5-1.6 第四級塩 2 石油類/ナシ
注意	クシ目チャ ナシ	リード散布 (カボトリッジガ ン)	自動及ビハンド パネーション
用	水質材料直 吸り	各種実機部品材	パネーション
特	フロン型	パネルジョイント 用	パネル後装用
性	非吸着性	無汚濁1級選	高選硬化型

表 3. 20~KU909S/W の稼働性能

銅合金系フローリングの接合性 (平均引張強度)			
試験項目	試験条件 (JIS 5521)	試験結果	規格
引張強度 $\sigma$ (N/cm <sup>2</sup> )	16 [1.7]	18 [1.9]	60 [5.2]
圧縮強度 $\sigma$ (N/cm <sup>2</sup> )	15 [1.6]	14 [1.5]	65 [5.6]
熱膨張係数 $\alpha$ (1/°C)	10 [1.1]	14 [1.5]	66 [5.6]
SI 単位換算係数	合格	合格	合格

※※※  
【処方量】：約550μ/m<sup>2</sup>，オーブンタイムは5分（20℃）

・出り合わせ可能時間・〔平面弓張試験〕

接合部の位置	材料	KUS05					KUS06				
		15分	30分	45分	60分	90分	15分	30分	45分	60分	90分
10℃×60%RH	—	—	—	—	—	—	54 [5.6]	54 [5.6]	49 [5.0]	58 [5.6]	58 [5.6]
20℃×60%RH	5.0 [5.2]	5.0 [5.2]	4.4 [4.5]	5.3 [5.5]	4.7 [4.8]	50 [5.2]	47 [4.8]	53 [5.5]	48 [4.9]	51 [5.1]	
30℃×60%RH	4.9 [5.0]	4.7 [4.8]	5.8 [6.0]	5.0 [5.2]	4.2 [4.5]	—	—	—	—	—	

据素材：特殊加工低発泡ポリエチレン裏打ちフロリーング/フレキシブルボード

接着強さの立ち上がり（平面引張試験）。

項目	K1000S						K1000W					
	22時間	24時間	36時間	48時間	72時間	120時間	24時間	36時間	48時間	72時間	120時間	
試験温度	5℃×60×8RH	22±2℃	24±1℃	50±5℃	49±5℃	51±5℃	22±2℃	45±4℃	50±5℃	48±4℃	51±5℃	
試験湿度	20℃×60×8RH	77±3%	47±4.8%	50±5.2%	49±5.1%	51±5.3%	20℃×60×8RH	44±4.5%	50±5.2%	48±4.9%	51±5.5%	
試験速度	30℃×60×8RH	37±3.8%	55±5.7%	53±5.5%	52±5.4%	51±5.3%	30℃×60×8RH	44±4.5%	50±5.2%	48±4.9%	51±5.5%	

被覆材：特殊加工低発泡ポリエチレン製打ちフロリング/フレキシブルボード

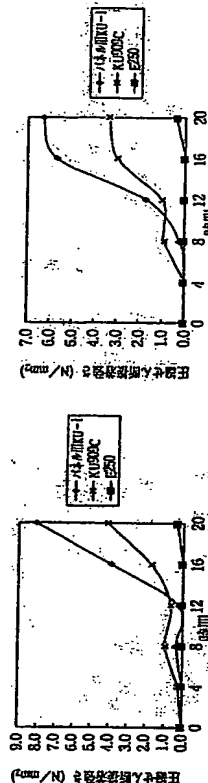
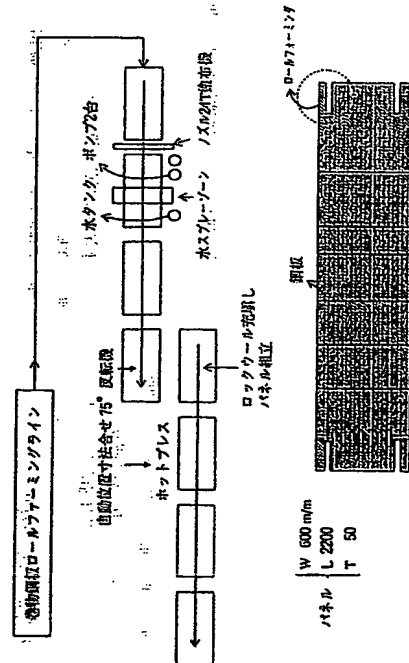


図3.23 0℃に於ける圧縮せん断接着力さ(米マツ)



図3.25 23℃に於ける圧縮せん断接着強さ (米マツ)



鋼板 0.75mm/m PVC化粧鋼板  
□777-1 501×100w×1.250L m/m

接着剤塗布量 ピーク値付25mmピッチで250g/m<sup>2</sup>

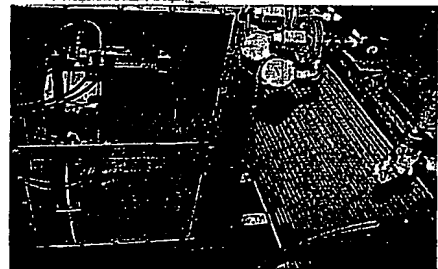
水玻璃 约30g/m<sup>2</sup>

プレス条件 70℃ 2分 0.1kg/cm<sup>2</sup>

ラインスピード 1枚毎7.5秒

### 図3.26 KU810FL/FSによるパネル製造概要





KU908S/Wの接着試験のデータ<sup>(1)</sup>を表3・20に本質的に、構造用接着剤パネルボンドKU-Iとエポキシ系接着剤ボンドE250との粘度別立上り接着強度の比較を図3・23～3・25に示す。

又自動塗布方式での KU810P<sub>L</sub>/PS のパネル製造  
概要例を図3.26~3.28に示す。

一 液態硬化型ウレタン系接着剤は通硬化・無発泡型の開発や他の樹脂との複合化により新しい機能を与える事により今後更に応用範囲が拡大すると思われる。

## 1) Polyurethanes Chemistry and Technology Part

3) “ポリウレタン樹脂ハンドブック”，岩田敬治編  
(日刊工業新聞社)。

4) 永田, (三洋化成工業株), 産業技術研究会七三  
昭和63年9月12日 (東京).

5) Janusz Kozakiewicz, *Adhesion* (GBR) 13, 114-141. (1989).

The map shows the northern Adriatic coastline of Italy. Key locations marked include Trieste, Udine, Gorizia, and Trieste. The map includes latitude and longitude coordinates. Sampling stations are indicated by numbers 1 through 10. The map also shows the location of the sampling stations relative to the coastline and the Adriatic Sea.

**図3.29** ジョールのジイソシアネートによる変性

### 3.4.1.2 イソシアネート原料

PU 溶剤の製造によく用いられるジソジンシアート類を表3・22にあげる。反応型二液 PU 溶剤の硬化剤として用いられる場合には、これらジソジンシアート類は、アダグド体・ビュレット体・トリブチルホスフィン・ブチルマリン酸に反応し、抽出あるいはメタノール抽出等の手段で未反応のジソジンシアートモノマーを除去して使用される。反応性の目的は、蒸気圧の低下・官能基数や NCO 含有量、粘度等の調整である。表3・23に各種硬化剤の構造をあげるが、低分子の MDI や Desmodur 等の蒸気圧が低い。

3.4.1 反応型二液PU接着剤の基本組成  
PU接着剤と言えどももちろん分子中にイソシア  
ネート(NCO)基と水酸(OH)基がもたらされるウ  
レタン(-NHCOO-)結合を有する接着剤と定義さ  
れるが、広義にはNCO化合物より誘導するすべ  
き接着剤を言うこともある。反応型二液PU接着  
剤では、アミン系樹のポリウレタン樹脂をエポキシ  
硬化剤とNCO化合物で硬化するタイプ(アルゴール樹脂)

• 武汉政工学院化学系 化学系第 1 研究室  
大邑市温江区三本町 2-17-85 号 532

ポリウレタン (PU) 接着剤は約50年前にバイエル社が Desmodur/Desmocol として上市して以来、インジネット化合物の多岐にわたる反応性、粘着性、弾性特性をはじめ優れた諸特性により年々その用途は広がってきた。今では、プラスチック・皮革・金属等に広く使用されており、その生産量も約3,300万トンと言われてゐる。PU接着剤がそのような多岐にわたる基材に幅広く用いられてゐるのは、インジネット基が富い反応性と弾性を有し、各種油性非水性化合物の特性を帯びた幅広い接着剤設計、ウレタン結合や炭素結合のもつ高い硬さ、圧力と温度面への物理的結合性による接着力の向上、防水・耐薬品性などの化学的性質に優れている点に加え、常温に近い温度でも硬化が可能なことによる。

反応型二液PU接着剤は、一般型と比べると、配合の手間・配合量のボタボタの問題はあるものの、接着面質性の点からは優位であり、アプリケーションターナー類の充実もありPU接着剤の主流を占めている。中でも最大の用途は、食品包装用ラミネート分野であり、金PU接着剤使用量の約1/2を占めている。

3.4.1 反応型二液PU接着剤の基本組成  
PU接着剤と言えどももちろん分子中にイソシア  
ネート(NCO)基と水酸(OH)基がもたらされるウ  
レタン(-NHCOO-)結合を有する接着剤と定義さ  
れるが、広義にはNCO化合物より誘導するすべ  
き接着剤を言うこともある。反応型二液PU接着  
剤では、アミン系樹のポリウレタン樹脂をエポキシ  
硬化剤とNCO化合物で硬化するタイプ(アルゴール樹脂)

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### 3.4 反応型二液ウレタン接着剤

夫照曜

系としてブリントラミ等の分野で実用化されている。ヤカルボン酸基含有ポリウレタン樹脂をカルボジイミド化合物やオキサンリン化合物等で変化するすることも検討されているが、基本的に分子中に吸収数の活性水素基（通常はOH基）を有する化合物——主剤一と、NCO基を有する化合物—変性剤—を、無溶剤のまま、あるいは溶剤に溶解して、あるいは水溶性にして用いる。さらに、用途に応じて無機充填剤や安定剤・触媒・接枝剤付与剤等添加剤を併用することもある。

3.4.1.1 活性水素化合物  
活性水素化合物にはアミンやカルボン酸、活性メチレン基をもつものもあるが、通常PU接着剤に使用される原料の大部分はOH系化合物である。接着剤に代換的な原料をあげる。反応型二液PU接着剤では、これらの化合物は主剤としてよく用いられる場合とジイソシアネートで変性し、分子重や粘度を調整して用いる場合とがある(図3.29)。

$$n \text{HO}-\text{R}-\text{OH} + (n-1) \text{OCN}-\text{R}'-\text{NCO} \rightarrow$$

**図3.29 ジョールのジイソシアネートによる変性**

### 3.4.1.2 イソシアネート原料

PU 溶剤の製造によく用いられるジソジンシアート類を表3.22にあげる。反応型二液 PU 溶剤の硬化剤として用いられる場合には、これらジソジンシアート類は、アダグド体・ビュレット体・トリブチルホスフィン・ブチルマゲネシウムに反応し、抽出あるいはメタノール抽出等の手段で未反応のジソジンシアートモノマーを除去して使用される。反応性の目的は、蒸気圧の低下・官能基数や NCO 含有量、粘度等の調整である。表3.23に各種硬化剤の構造をあげるが、低分子の MDI や Desmodur RP 等の蒸気圧が低い。

# Appendix B

Translation

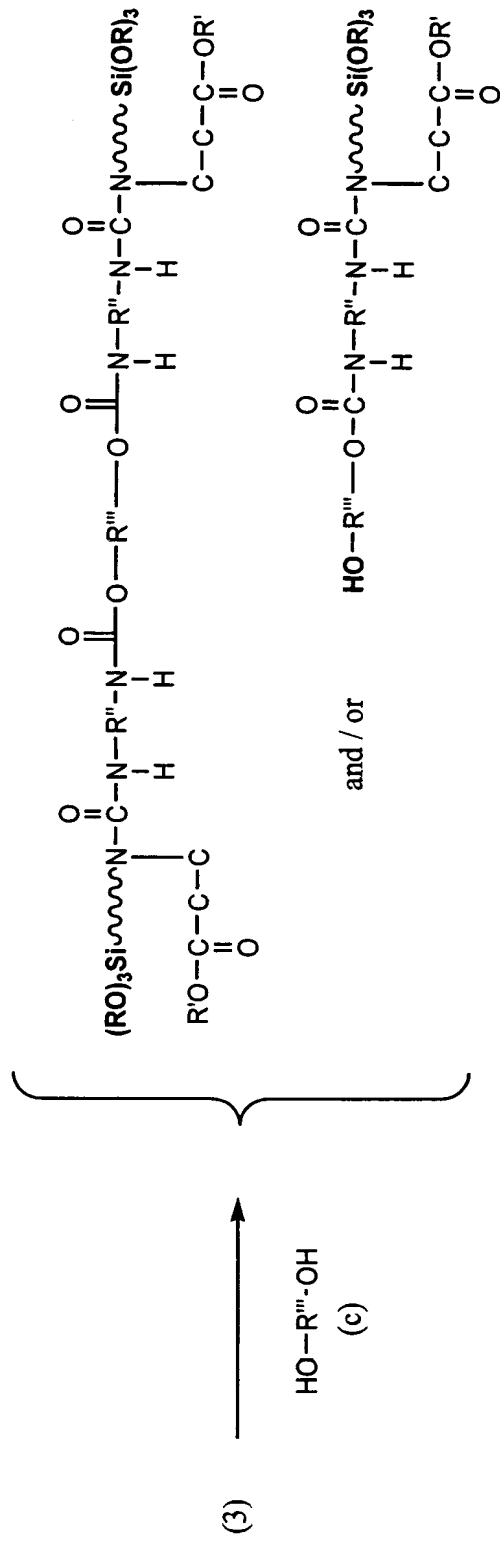
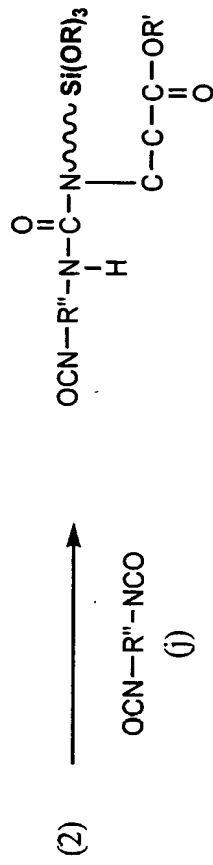
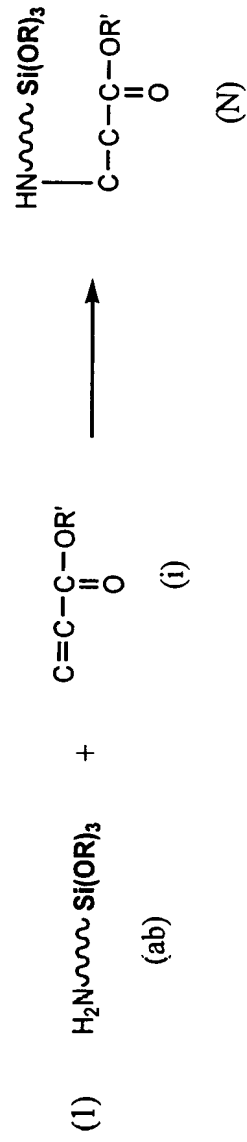
Table 3.18 Effect of Isocyanate Group Content On Molecular Weight Of Prepolymer

GPC chart Mobile phase: THF Flow rate: 1 ml/min	(a)	(b)	(c)
Isocyanate group content	15%	9%	6%
Peak No. (composition)	Molecular weight converted with polystyrene		
8 pre trimer	—	5760	6000
7 pre dimer	4310	4310	4450
6 Basic unit	2550	2560	2640
5	—	—	—
4 iso tetramer	529	541	565
3 iso trimer	446	456	476
2 iso dimer	361	368	383
1 iso monomer	253	259	271
Number average molecular weight	567	690	1402
Weight average molecular weight	1657	2910	4549
Viscosity mPa·s [25°C]	5900	13000	15800

\* Polymeric MDI prepolymer

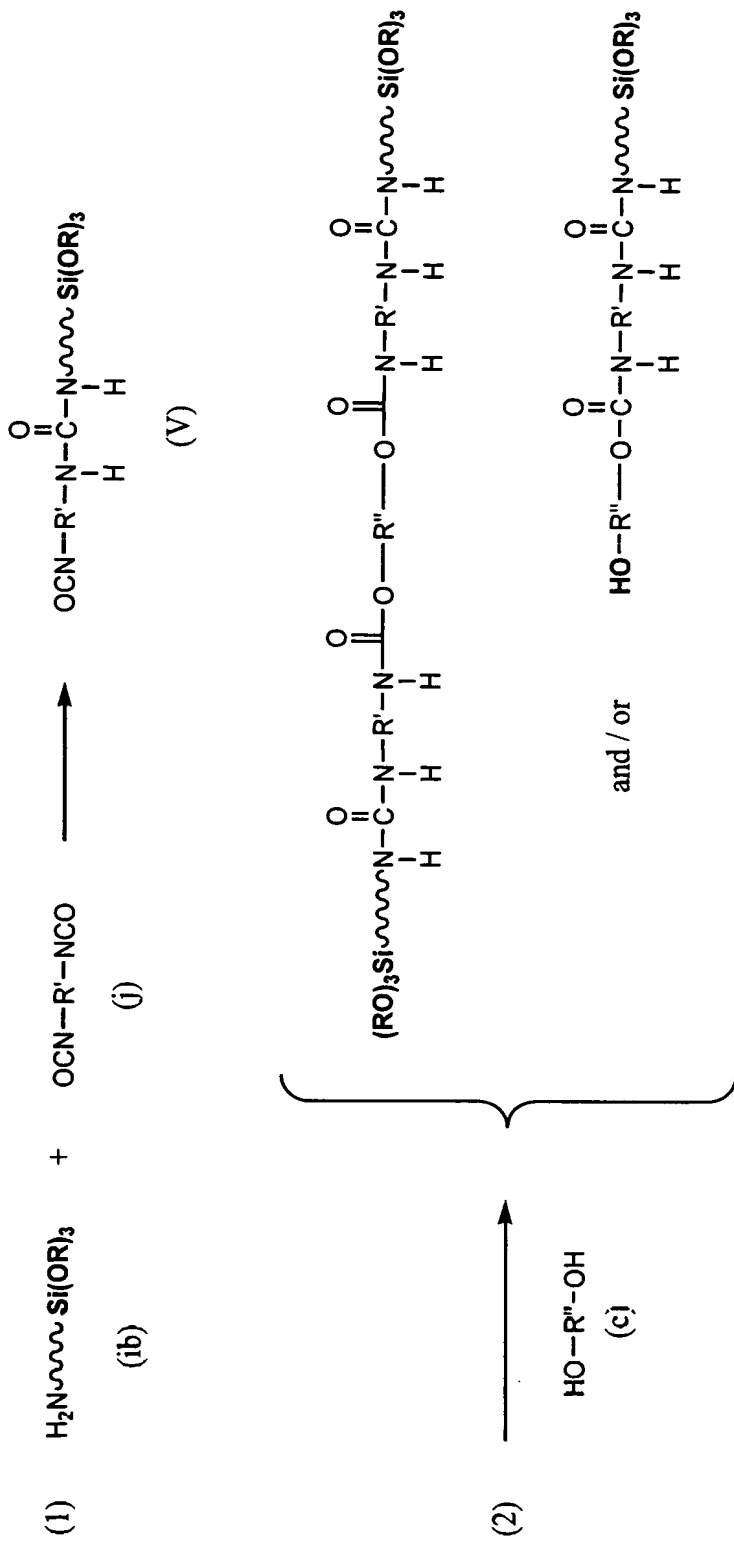
# Appendix C

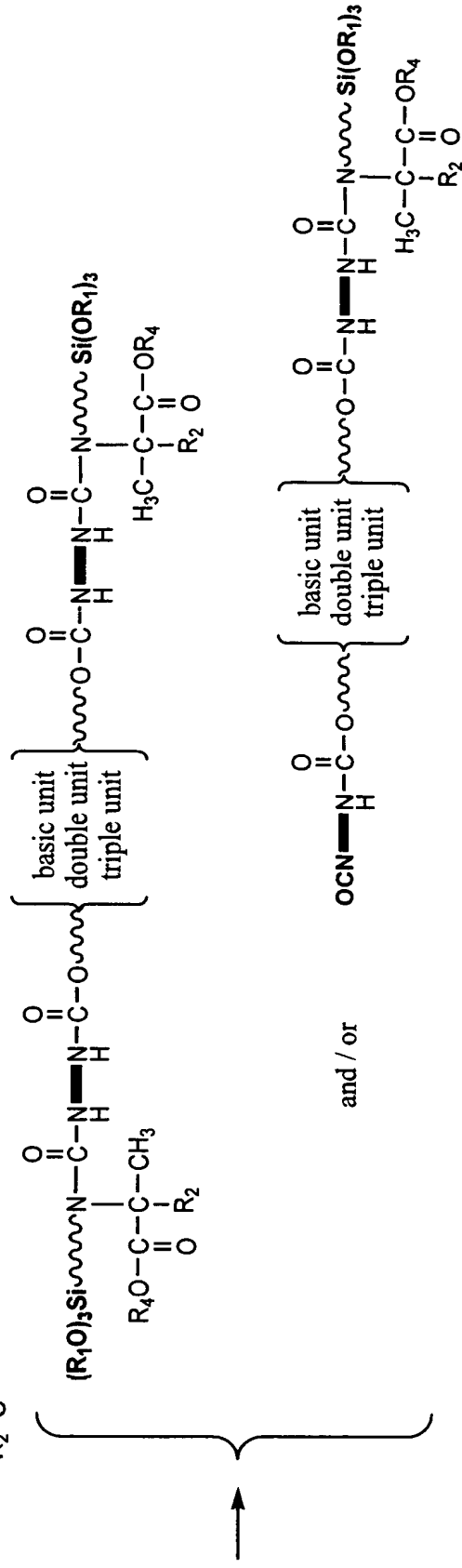
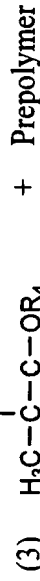
## Claim 46



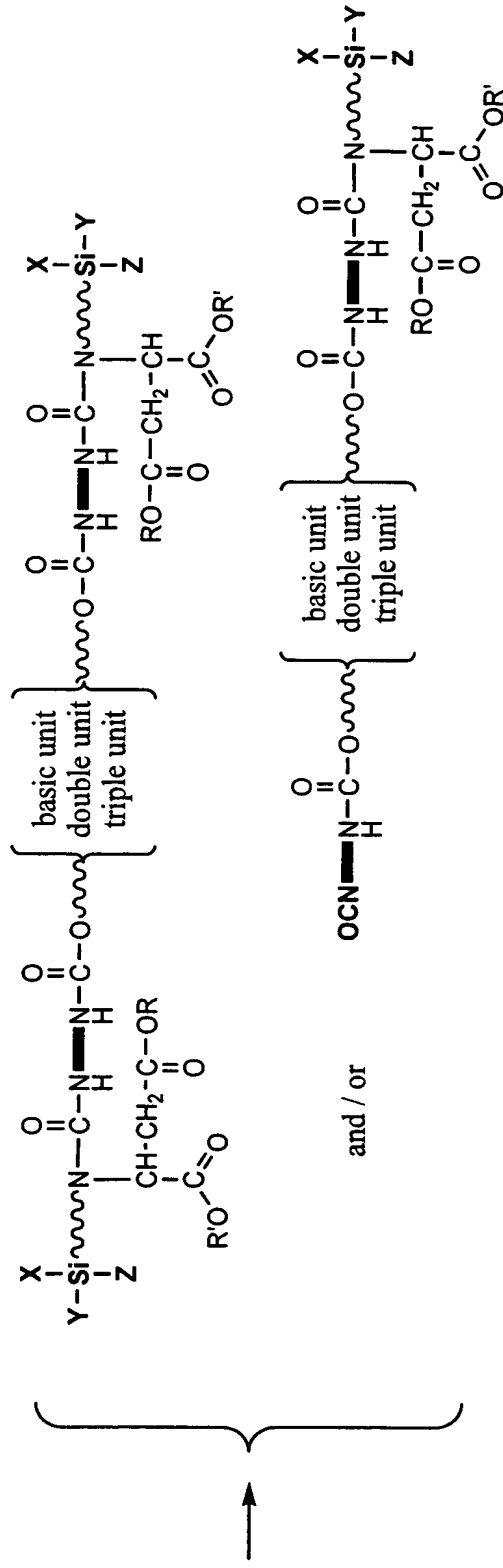
## Appendix D

### Claim 50



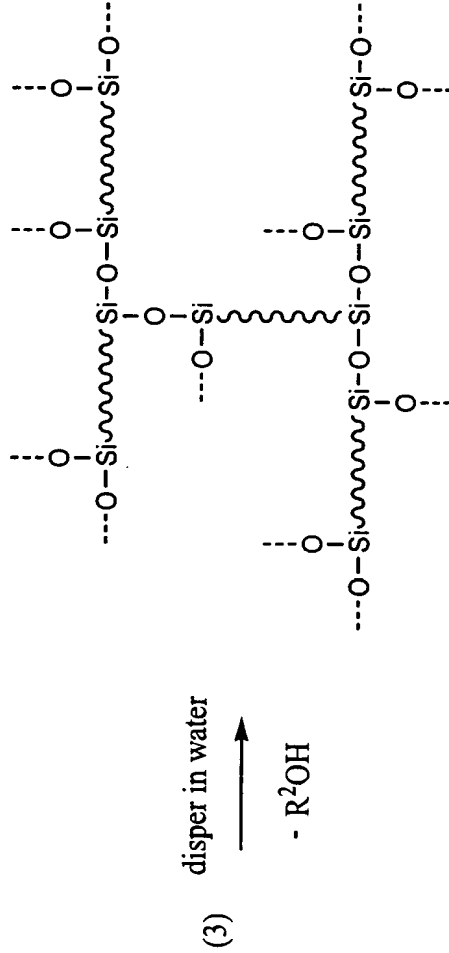
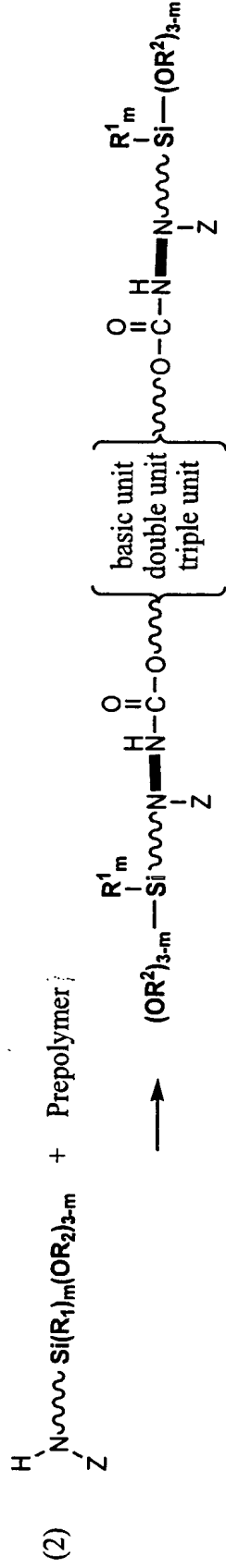
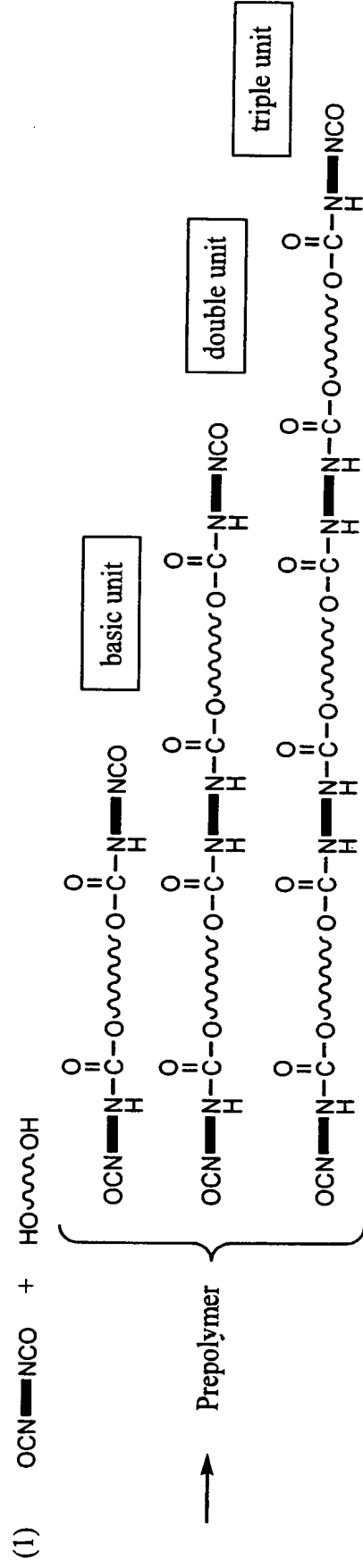
Barron

## Zweiner



# Krafcik

## Appendix G



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